



Simultaneous Extraction and Separation of Oil and Azadirachtin from Seeds and Leaves of *Azadirachta indica* using Binary Solvent Extraction

Sheela Subramanian¹, Aiza Syuhaniz Salleh¹, Robert Thomas Bachmann^{1,*}, and Md. Sohrab Hossain²

¹Branch Campus Malaysian Institute of Chemical and Bio-Engineering Technology, Green Chemistry & Sustainable Engineering Technology Cluster, Universiti Kuala Lumpur, 78000 Alor Gajah, Malacca, Malaysia

²Division of the Environmental Technology, School of Industrial Technology, Universiti Sains Malaysia, 11800 Penang, Malaysia

Abstract – Conventional extraction of oil and azadirachtin, a botanical insecticide, from *Azadirachta indica* involves defatting the seeds and leaves using hexane followed by azadirachtin extraction with a polar solvent. In order to simplify the process while maintaining the yield we explored a binary extraction approach using Soxhlet extraction device and hexane and ethanol as non-polar and polar solvents at various ratios and extraction times. The highest oil and azadirachtin yields were obtained at 6 h extraction time using a 50:50 solvent mixture for both neem leaves (44.7 wt%, 720 mg_{Aza}/kg_{leaves}) and seeds (53.5 wt%, 1045 mg_{Aza}/kg_{seeds}), respectively.

Keywords – Azadirachtin, limonoids, neem oil, binary solvent extraction, botanical insecticide

Introduction

The neem tree (*Azadirachta indica*) is an evergreen tropical plant originating in South Asia but increasingly encountered in Africa, America and Australia. It belongs to the *Meliceae* family, grows rapidly in tropic and semi-tropic climate with an extended dry season, and is used in many countries for afforestation, fuelwood production as well as an avenue or shade tree.¹⁻³ All parts of the neem plant such as leaves, seeds, bark, flowers, fruit and root are useful with applications in toiletries, pharmaceuticals, furniture manufacturing, cattle and poultry feeds, nitrification of soils for various agricultural crops, and pest control.^{2,4} Of all plant components however, neem seed oil and its constituents have attracted by far the greatest interest over the past few decades.⁵

The ripe neem fruits contain light - coloured seeds that comprise of up to 50 wt% oil, which has been used for birth control and to treat diseases such as diabetes, cancer and heart failure.⁶ Neem seed oil is also applied in agriculture as botanical pesticide, insecticide and fungicide, while it has its importance in cosmetic products such as shower gel, acne care and shampoo.⁶⁻⁸ The oil can further-

more be used to extend the leather goods.³ Neem seed oil mainly yields quercetin and nimbosterol as well as a number of other limonoids such as azadirachtin, nimbin and its derivatives.⁴ Among the various limonoid components, azadirachtin is the most important biologically active component which has many anti-infective, anti-bacterial, antifungal and antimicrobial properties.⁹ Three derivatives of azadirachtin are currently known of which azadirachtin is the most abundant (80%) and biologically active compound used as commercial botanic insecticide.¹⁰ While azadirachtin impairs the insect growth regulatory system in all species tested, the effectiveness varies depending on insect order and species.⁷ Since azadirachtin does not kill adult insects, neem-based insecticides tend to be used with other strategies or beneficial pests.

Table 1 summarizes the extraction of neem oil and azadirachtin from neem seeds and leaves using Soxhlet extraction under various experimental conditions. Soxhlet extraction is a solid-liquid process commonly used to obtain oil from seeds and other plant components.¹¹ Solvent selection is important to provide a good yield from the extraction. The solvent typically used for oil extraction is n-hexane due to its high stability, boiling point, non-polarity, low corrosiveness and high oil yield.^{2,3,12} Oil yield further depends on moisture content, extraction time, size of particle and solvent:solid ratio.¹³ In the case of azadirachtin, a combination of n-hexane extraction to remove oil followed by ethanol extraction of

*Author for correspondence

Robert Thomas Bachmann, Branch Campus Malaysian Institute of Chemical and Bio-Engineering Technology, Green Chemistry & Sustainable Engineering Technology Cluster, Universiti Kuala Lumpur, 78000 Alor Gajah, Malacca, Malaysia.
Tel: +606 551 2157; E-mail: bachmann@unikl.edu.my

Table 1. Oil and azadirachtin yield from neem seeds and leaves using solvent extraction under various process conditions

Component	Solvent	Seed : solvent ratio (g : mL)	Extraction time (h)	Particle size (mm)	Oil yield (wt%)	Azadirachtin yield (wt%)	References
Seed	n-Hexane ¹	1 : 4 ¹	4 ¹	NA	46.7	0.25	14
	Ethanol ²	1 : 5 ²	4 ²				
	n-Hexane	NA	8	NA	45	0.23	15
	n-Hexane	1 : 7.8	NA	<1.41	NA	0.06	18
	Methanol	1 : 7.8	NA	<1.41	NA	0.15	18
	Petroleum-ether	1 : 3.3	1 - 3	0.425 - 2.38	11.5	NA	16
		1 : 6.1			47.3		
		1 : 16.7			37.5		
	Hexane	1 : 15	2 - 6	0.6 - 1.4	40	NA	12
	n-Hexane	1 : 5	2 - 6	0.425 - 0.710	43.5	NA	2
	n-Hexane	1 : 5	6	0.425 - 1.4	44.3	NA	3
	Ethanol				41.1		
	n-Hexane	1 : 15	2 - 8	0.25	45.4	NA	17
	Ethanol				46.4		
	Hexane	1 : 15	6	0.355 - 1.0	40.4	NA	1
	Ethanol				42.7		
	Methanol				42.9		
	Ethanol + Hexane				43.7		
	Ethanol	1 : 10	6	0.425 - 0.71	40	NA	11
Leaf	Ethanol	1 : 10	6	0.425 - 0.71	36	NA	11

¹ - oil extraction, ² – azadirachtin extraction from defatted neem seed

azadirachtin from defatted neem seed cake has been reported¹⁴ (Table 1). The authors obtained an oil yield of 52.5% (v/w), while ethanol extraction and subsequent purification steps resulted in recovery of 5 g of azadirachtin from about 950 g of defatted neem seed cake.¹⁴ Another study investigated the effect of various solvents and found that polar solvents extract more azadirachtin than non-polar solvent extracted from n-hexane defatted neem seeds suggesting solvent mixing maximizes azadirachtin yield¹⁹. The majority of authors suggested to use a 1:15 solid to solvent ratio and preferred a particle size range of 0.425 – 0.71 mm. The extraction was carried out within 2 to 8 h with 6 h the most common extraction time (Table 1). In terms of solvent choice, most authors selected n-hexane followed by ethanol, petroleum-ether and more recently ethanol:n-hexane mixtures for single-step oil and azadirachtin extraction from neem seeds. A similar solvent preference for solvents can be observed for extraction from neem leaves. In a recent study the oil yield from neem seed and leaves was determined and compared under non-optimized process conditions¹¹ while another study reported the extraction of azadirachtin from neem seed oil and defatted neem seeds.¹⁴

Binary solvents were suggested to be more environmentally friendly, less toxic and give greater oil yields from neem seeds compared to single solvent extraction

using hexane for primary and ethanol for secondary extraction (Table 1). Sequential single solvent extraction also increases heat stress to other valuable non-oil seed components such as proteins and carbohydrates with detrimental consequences to their quality and economical value.

The present study was therefore conducted to extract neem oil and azadirachtin from neem leaves and seeds using Soxhlet extraction in a binary solvents system. Subsequently, the azadirachtin was separated from the extracted oil using high performance liquid chromatography (HPLC). Soxhlet extraction experimental conditions were optimized by evaluating the interaction effects between extraction time and binary solvent ratio on maximum neem oil and azadirachtin yield.

Experimental

General experimental procedures – The separation of azadirachtin from extracted neem seed and neem leaf oil was conducted using HPLC. A 0.5 mg Sigma A7430 azadirachtin standard was used to calibrate the HPLC. The azadirachtin standard was diluted in 5 mL methanol (Merck, HPLC grade) as stock solution (100 ppm) and further diluted with methanol to 20 ppm. A Perkin-Elmer system comprising of series 200 pump and series 200 UV-

VIS detector set at 215 nm absorbance was used. The mobile phase consisted of an acetonitrile: water mixture of 72.5:27.5 (v/v) with mobile phase temperature of 45 °C using column C18 of 250 mm × 4.6 mm id × 5 µm. A known weight of neem oil was dissolved in methanol at a sample to solvent ratio of 1:10 (w/v) and sonicated until complete solubilization. Then, the mixture was filtered through a Millipore 0.45 µm membrane syringe filter before injection of 20 µL into the HPLC. The mobile phase flow rate was 1 mL/min. The retention time for azadirachtin was 15.85 min with an isocratic elution time of 20 min. The HPLC was flushed after every 10 samples. A quality control was included using methanol injection at the beginning and after 5 samples.²⁰

Plant materials – Fresh neem leaves were collected from a 12 years old neem tree located at Mambau, Malaysia and identified by one of the authors (S.S.). The neem seeds were procured from Tamil Nadu, India.

Preparation of leaves – Fresh leaves were soaked in tap water (1:2 w/v ratio) for 24 min at room temperature in order to remove impurities such as dust and any unwanted metals. The soaked neem leaves were then rinsed, dried at 50 °C for 48 h and the moisture content determined using Eq. 1.

$$\text{Moisture content (\%)} = \frac{W_1 - W_2}{W_1} \times 100\% \quad (1)$$

where W_1 is weight of neem leaves before drying [g], W_2 is the weight of neem leaves after drying.

The dried neem leaves were finely chopped and ground using a blender with dry mill cup (Panasonic, MC-GM 1011H) to increase the surface area and speed up the extraction process.²¹ Ground neem leaves were sieved (Endecott) to obtain a particle size range of 425 to 710 µm. The neem leaves powder was stored in a vacuumed airtight container in the dark at room temperature to prevent oxidation and contamination of neem leaves powder.

Preparation of seeds – The seeds were cleaned to remove any sticks, unwanted leaves, bad seeds, sand and dirt to ensure oil produced is not contaminated and of

high quality. The cleaned neem seeds were dried at 55 °C for 72 h until constant weight, and the moisture content determined by following the Eq. 1. The dried clean neem seeds were dehulled by hand followed by roasting for about 5 min to enhance oil extraction. The roasted neem seeds were crushed in a blender and sieved to obtain particles ranging from 425 and 710 µm in size. The sieved neem powder was then stored under vacuum in an airtight container at 4 °C prior to use.⁹

Extraction and isolation – Ethanol (Merck, HPLC Grade) and n-hexane (Merck, HPLC Grade) were used as single and binary solvents in the Soxhlet extraction process. Soxhlet extraction (Buchi Extraction System2, B-811) was carried out with 4 units per run. Ten gram of sample was weighed, placed into a pre-weighed thimble (Whatman No. 41) and the total weight recorded. A folded filter paper was inserted carefully into the top of the thimble to prevent sample loss. Subsequently, 150 ml of the pre-heated solvent was poured into each extractor flask representing a mass to solvent ratio of 1:15 (w/v). Extraction was carried out under various process conditions summarised in Table 2. At the end of the extraction process, the units were allowed to cool down for 30 min and weighed. The solvent-oil mixture was poured into a round bottom flask and transferred to a rotary evaporator (Büchi, R200) operated at 80 °C to remove the solvent. The recovered oil inside the flask was weighed and stored in a vacuumed air tight glass vial at 15 °C for further analysis. The neem oil yield was calculated using Eq. 2. Experiments were carried out in triplicate.

$$\text{Extraction yield (\%)} = \frac{M_1 - M_2}{M_1} \times 100\% \quad (2)$$

where M_1 is the mass neem seed or neem leaves before extraction and M_2 is the mass of the neem seed or neem leaves after extraction.

Statistical analysis – Experimental data were processed using Excel to determine the arithmetic mean as well as the standard deviation. Two-way ANOVA and determination of the interaction effects between extraction time

Table 2. Parameters used for Soxhlet extraction

Parameters					
n-hexane to ethanol ratio (v/v)	100 : 0	60 : 40	50 : 50	40 : 60	0 : 100
Soxhlet temperature (°C)	70	70	70	70	80
Soxhlet heating mode	10	10	10	10	16
Time (hr)			3, 4, 5 and 6		
Particle size range (mm)			0.425 – 0.710		
Mass to solvent ratio (g/ml)			1:15		

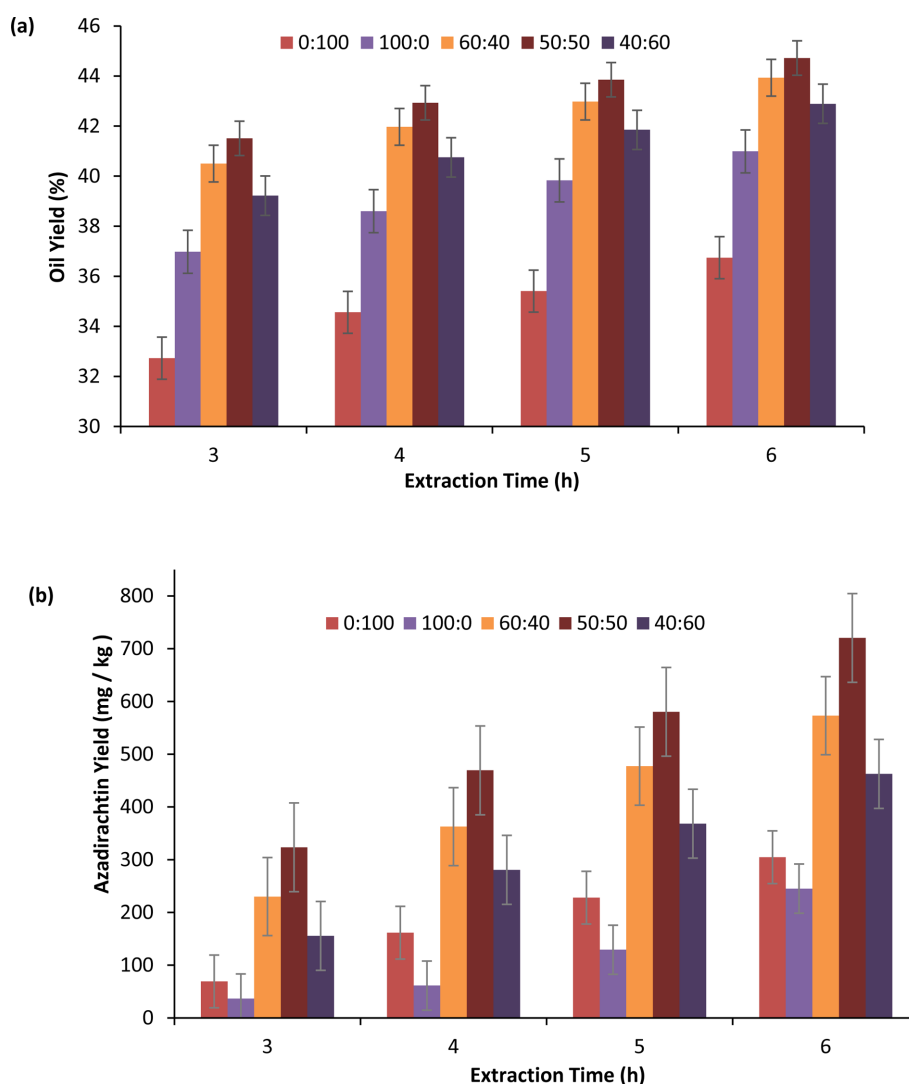


Fig. 1. Neem oil yields (a) and azadirachtin yields (b) from neem leaves at various solvent ratios and extraction times ($n=3$).

and solvent ratio was performed using MINITAB software (ver. 16.1) at 95% confidence level.

Results and Discussion

Soxhlet extraction of oil and azadirachtin from neem leaves was carried out using pure n-hexane and ethanol as well as various binary solvent mixtures as shown in Fig. 1. It was observed that binary solvent had a higher affinity for neem oil and azadirachtin from neem leaves at the studied solvent ratios and extraction times. The highest oil and azadirachtin yields were about 45% and 720 mg/kg, respectively, at a solvent ratio of 50:50 for 6 h extraction time. In the case of single solvent using ethanol (ratio 0:100) and n-hexane (100:0), the pure n-hexane had a higher oil yield (41.0%) compared to the pure ethanol

(36.7%). Conversely, the extracted azadirachtin yield from neem leaves was higher using ethanol as single solvent. The extraction using the single solvent n-hexane and ethanol resulted in 11 ± 1 wt% and 24 ± 2 wt% lower oil yields compared to the binary solvent ratio of 50:50 at extraction time of 6 h. The ethanol-based oil yield is in excellent agreement with literature¹¹ which reported a similar yield using same extraction time and particle size range (Table 1). Oil yield was found to increase linearly ($R^2 > 0.98$) with extraction time regardless of single or binary solvent system suggesting that maximum oil recovery may be achieved at extraction times greater than 6 h.

Azadirachtin yield obtained from neem leaves in single solvent extraction using n-hexane and ethanol were 2.7 to 7.8 times and 1.9 to 3.7 times lower than the maximum

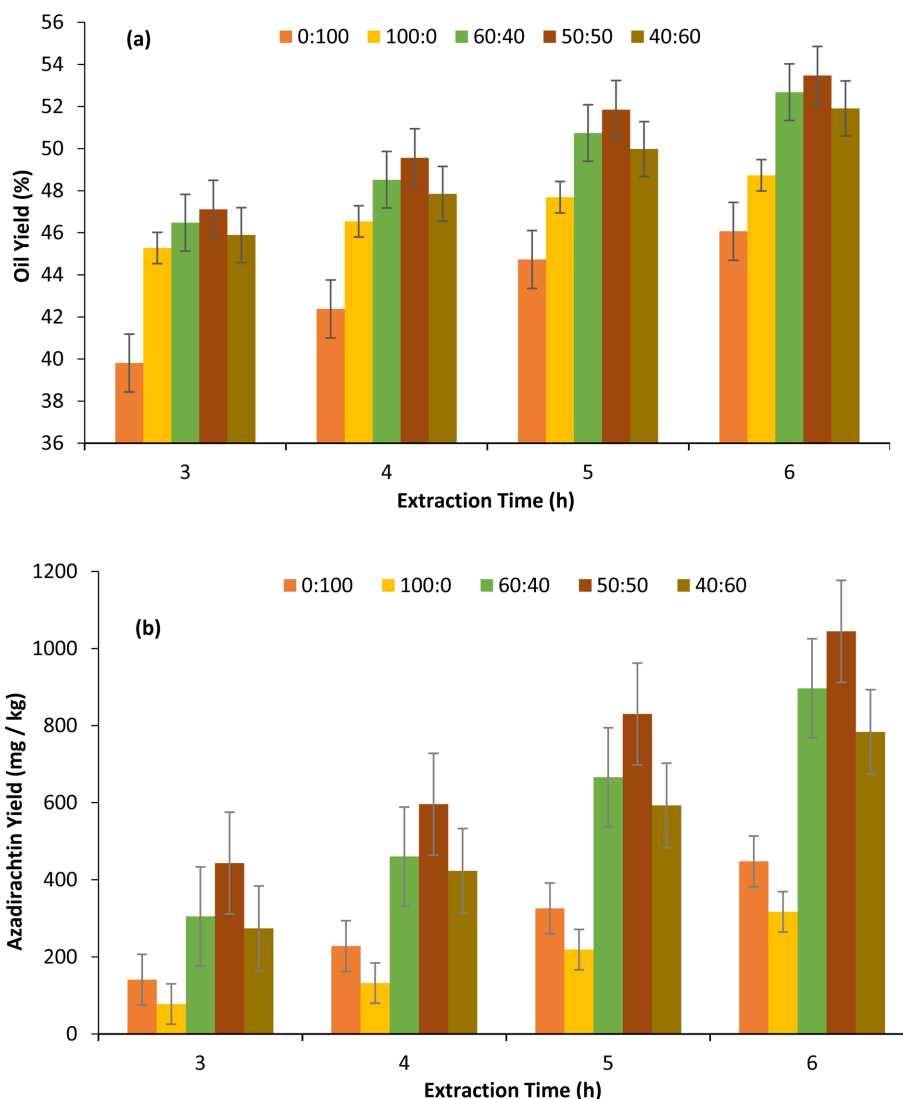


Fig. 2. Neem oil yield (a) and azadirachtin yields (b) from neem seeds at various solvent ratios and extraction times ($n=3$).

azadirachtin concentrations at binary solvent ratio of 50:50 (n-hexane:ethanol). This suggests that azadirachtin is relatively more soluble in polar than non-polar solvents.¹⁹ The highest yield of azadirachtin from neem leaves was found to be 720 mg/kg using a binary solvent mixture of 50:50 at 6 h extraction time. It has been reported that polar solvents such as ethanol and isopropanol can remove phospholipids from the plant cell wall which in turn improves oil permeability and thus facilitates a faster extraction.²³ Increased phosphatide levels in the extracted oils can be advantageous for the down-stream processing of the defatted neem seed meal but problematic in terms of extracted oil quality requiring a more rigorous degumming step.

Extraction of oil and azadirachtin from neem seeds was

carried out using n-hexane and ethanol varying extraction time and solvent ratio (Fig. 2). The highest oil yield obtained was 53.5% using a binary solvent system of 50:50 followed by 60:40, 40:60, 100:0 and 0:100 (Fig. 2a), while the highest azadirachtin concentration was 1045 mg/kg with the binary solvent system of 50:50 followed by 60:40, 40:60, 0:100 and 100:0 (Fig. 2b).

The use of n-hexane as the sole solvent (solvent ratio 100:0) resulted in a 7 ± 1 wt% lower oil yield compared to solvent ratio of 50:50, while ethanol yield was 17 ± 2 wt% lower, which, as far as single solvent extraction performance is concerned, confirms similar trends reported in literature (Table 1). However, some authors^{1,17} observed slightly greater oil yields for ethanol extraction (Table 1). While particle size range and seed:solvent ratio were

Table 3. Two way ANOVA of the neem oil and azadirachtin extraction from neem seeds and neem leaves. All values are F values with significance level P as indicated by asterisks

Factor	Neem Seeds		Neem leaves	
	Neem oil	Azadirachtin	Neem oil	Azadirachtin
Time (h)	39.65*	270.95*	1573.19	2563.79*
Solvent Ratio	43.34*	272.42*	5758.06*	3117.48*
Time* Solvent Ratio	0.42	4.53*	3.20*	26.58*
R ²	0.9370	0.9899	0.9993	0.9990
R ² _{adj}	0.8771	0.9803	0.9986	0.9981

* p < 0.05

similar, variations may arise due to different temperature settings used which influences the number of extraction cycles in Soxhlet and the solubility of oil in ethanol. The working condition and degree of automation of the Soxhlet instrument used are also affecting the performance, while the purity of the ethanol has also not been reported by the authors. It cannot be ruled out that some laboratories used denatured ethanol for seed defatting for economic reasons. In such cases the presence of methanol or other denaturing agents can affect the oil extraction yield. Seasonal and geographic variations are also known to affect the composition of plant products²² and may thus also account for the observed deviation.

The extra 7% yield attained with the binary solvent system is attributed to the removal of phospholipids which enhanced oil permeability and thus yield as discussed earlier. An increase in extraction time from 2 to 6 h resulted in a linear oil yield increase ($R^2 > 0.99$) regardless of solvent system used. The oil yield after 6 h of n-hexane extraction was 5% greater than reported elsewhere.² However, these authors used a lower seed: solvent ratio which, everything else equal, is expected to result in a lower oil recovery (Table 1).

Azadirachtin concentration in n-hexane-extracted neem oil was 3.0 to 5.5 times lower than the maximum concentration obtained with the 50:50 n-hexane:ethanol solvent mixture, whereas pure ethanol extracted neem oil contained 2.0 to 2.7 lower azadirachtin concentrations. This follows a similar trend as observed with neem leaves confirming that azadirachtin is relatively more soluble in polar than non-polar solvents which also agrees with observations reported in literature.^{14,18} The concentration of azadirachtin in neem seed oil increased linearly with extraction time ($R^2 > 0.98$) and reached comparatively high concentrations (Table 1). The highest yields of azadirachtin from neem seed were found to be 317 mg/kg for n-hexane (6 h), 448 mg/kg for ethanol (6 h) and 1045 mg/kg for 50:50 binary solvent mixture (6 h), which

falls within the range of 300 to 2500 mg/kg suggesting that the variability is caused by the extraction technology used, climate and geographic location.²¹

Our results agree with literature reporting that the azadirachtin concentration decreased in the order of seed kernels > leaves > bark > roots > stem.²⁴ Comparing the highest azadirachtin yield from neem seeds with leaves it is suggested that neem seeds are the primary source for commercial azadirachtin production.

The colour of neem leaf oil was dark greenish-brown probably due to presence of chlorophyll. The colour of neem seed oil extracted using ethanol was darker than neem seed oil extracted using n-hexane and binary solvents. A golden to dark golden appearance was noted for neem seed oil which agrees with a study investigating and comparing the physico-chemical variation of 42 ecotypes in India.¹⁵ The neem leaf oil was found to be less viscous. Besides that, the odour of neem seed oil was stronger (peanut - garlic mixed smell) compared to neem leaf oil (pungent smell) probably due to presence of sulphurous compounds and chlorophyll, respectively. The texture of neem seed oil was smooth and neem leaf oil was silky which agreed with literature.²⁰

The analysis of the two way ANOVA is presented in Table 3. The presence of interaction between solvent types and extraction time means that the way oil yield and azadirachtin concentration changes for different solvents depends on the extraction time and vice versa. Thus, both solvent types and extraction time is needed, as well as their interaction, to generate yield for oil and azadirachtin.

Two way ANOVA of all extraction experiments has shown that the R^2 and R^2_{adj} were at least 0.94 and 0.87, respectively. It is generally recommended that the R^2 value should be ≥ 0.80 for a good fitted model.²³ Nonetheless, a large R^2 value does not necessarily indicate an adequate model. Therefore, it is equally important to predict the R^2_{adj} value for a model, which gives a more appropriate evaluation of model adequacy.

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